In the claims:

Please amend the claims as shown below:

1. (Currently amended) A method for the dilution of dewatered and compressed cellulose pulp that has been consolidated into large pieces, where the dewatered cellulose pulp maintains a first consistency greater than 20%, ~~preferably greater than 25%, and even more preferably greater than 30%, whereby~~ comprising:

fragmenting the cellulose pulp ~~is fragmented~~ into a finely divided pulp after or in association with dewatering, ~~c h a r a c t e r i s e d i n~~

granulating ~~that~~ the cellulose pulp ~~is granulated~~ through fragmentation to a particle size with a normal distribution with a maximum size that is less than 40 mm, ~~preferably less than 30 mm, and even more preferably less than 20 mm, and that during fragmentation maintains~~

while fragmenting, maintaining a consistency of the cellulose pulp that is essentially equivalent to the first consistency,

feeding ~~that~~ the cellulose pulp that has been finely divided through the fragmentation ~~is fed out~~ into a freely falling flow,

adding ~~that~~ dilution fluid ~~is added~~ under pressure towards the freely falling fragmented pulp through a number of fluid jets ~~(62)~~ arranged in association with the flow of the freely falling fragmented pulp,

~~that~~ the amount of dilution fluid added through the ~~said~~ fluid jets ~~(62)~~ ~~establishes~~ establishing a second consistency of the cellulose pulp in ~~the~~ a medium-consistency range 8-16%,

feeding ~~that~~ the cellulose pulp at this medium consistency 8-

16% ~~is fed onwards~~ onwardly to subsequent treatment stages, ~~that the~~ a dilution of the freely falling pulp ~~down to a medium consistency of 8-16% before it the freely falling pulp is fed onwards onwardly to subsequent treatment stages takes~~ taking place essentially exclusively under ~~the~~ an influence of hydrodynamic effect from the addition of the dilution fluid through the ~~said~~ fluid jets, and where no mechanical agitation ~~takes~~ taking place between the fragmentation of the cellulose pulp and ~~the~~ an underlying surface (Liq_{LEV}) of the cellulose pulp that has been diluted by the dilution fluid ~~that has been established~~.

2. (Currently amended) The method according to claim 1, ~~c h a r a c t e r i s e d i n that~~ wherein the fluid jets are arranged around the flow of fragmented pulp formed in the free fall, and are directed principally radially inwards towards the flow.

3. (Currently amended) The method according to claim 1, ~~c h a r a c t e r i s e d i n that~~ wherein the cellulose pulp at medium consistency is fed ~~onwards~~ onwardly to subsequent treatment stages through pumping.

4. (Currently amended) The method according to ~~either claim 1 or claim 2, c h a r a c t e r i s e d i n that~~ claim 1 wherein the dilution fluid added is added to a degree of more than 50%, ~~preferably more than 75-90%,~~ through the ~~said~~ fluid jets ~~(62)~~.

5. (Currently amended) The method according to ~~any one of claims 1-3, c h a r a c t e r i s e d i n that~~ claim 1 wherein the addition of dilution fluid from the ~~relevant~~ fluid jets ~~(62)~~ takes place in ~~the~~ a form of pressurized

~~pressurised~~ fluid jets that are directed obliquely ~~downwards~~ downwardly in ~~the~~ a fall direction ~~of fall~~ of the cellulose pulp.

6. (Currently amended) The method according to claim 4, ~~c h a r a c t e r i s e d i n that~~ wherein the fluid jets are directed at an angle of 45° ± 15° relative to ~~the~~ a vertical direction and ~~the~~ a fall direction ~~of fall~~ of ~~the~~ granulate.

7. (Currently amended) A device for the dilution of dewatered cellulose pulp, comprising:

shredder screw means for fragmenting pulp to a particle size in an interval of 5-40 millimeters, the shredder screw means having an outlet defined therein, the shredder screw means containing the fragmented pulp,

a vertical standpipe connected to the outlet of the shredder screw means, the standpipe carrying a flow of the fragmented pulp flowing under free fall, the standpipe having a distribution chamber defined therein at an upper end of the stand pipe, the distribution chamber arranged concentrically around the standpipe,

at least four nozzles arranged around a circumference of the distribution chamber, the nozzles being oriented inwardly towards a center of the flow to add a dilution fluid under pressure into the stand pipe, the nozzles being disposed above a liquid level of diluted pulp established in the standpipe,

a feed arrangement disposed at a bottom of the standpipe for

feeding the pulp to subsequent treatment stages,
a pump disposed at the bottom of the standpipe and in operative engagement with the feed arrangement, and
the standpipe having no mechanical agitator disposed above the liquid level.

~~dewatering equipment (7,80) to which pulp at an initial consistency in the range 4-12% has been fed and in which the cellulose pulp after dewatering maintains a consistency greater than 20%, preferably greater than 25%, and even more preferably greater than 30%, whereby the cellulose pulp is fed to fragmentation equipment (8, 8b) to be fragmented into a finely divided pulp, characterised in~~
~~that the cellulose pulp is granulated through fragmentation in the fragmentation equipment (8, 8b) into a particle size with a normal distribution with a maximum size that is less than 40 mm, preferably less than 30 mm, and even more preferably less than 20 mm,~~
~~that the pulp that has been finely divided is fed from the outlet of the fragmentation equipment into an essentially vertical stand pipe (22/40'), under free fall,~~
~~that a number of nozzles (62) are arranged around the circumference of the stand pipe (22), from which nozzles dilution fluid (LiqDIL) is added under pressure into the stand pipe and above a level (LiqLEV) of diluted cellulose pulp established in the stand pipe,~~
~~where the amount of added dilution fluid (LiqDIL) establishes~~

~~a consistency of the cellulose pulp in the range of medium consistency 8-16% and that this added amount, to more 50%, preferably to more than 75-90%, is added through the said nozzles (62) arranged above a level (LiqLEV) established in the stand-pipe,~~

~~that the cellulose pulp at this medium consistency is fed onwards to subsequent treatment stages by a feed arrangement (41),~~

~~that the dilution of the pulp to a medium consistency of 8-16% in the stand pipe takes place exclusively under the influence of hydrodynamic effect from the addition of dilution fluid through the said nozzles and without the use of a mechanical agitator above the level (LiqLEV) of fluid established in the stand pipe (22/40´)~~

8. (Currently amended) The device according to claim 7 ~~c h a r a c t e r i s e d i n that~~ wherein the device has ~~the cellulose pulp at this medium consistency is fed onwards to subsequent treatment stages for the cellulose pulp with a~~ the pump ~~(41)~~ connected to the stand pipe ~~(22/40´)~~ at ~~its~~ a lower part thereof close to the bottom of the stand pipe~~,~~ under the liquid level ~~(LiqLEV) of fluid established~~.

9. (Currently amended) The device according to claim 7 ~~c h a r a c t e r i s e d in that~~ wherein the nozzles ~~at least four nozzles~~ are arranged around ~~the~~ a periphery of the stand pipe, where ~~the~~ a distance between neighbouring nozzles is less than 50-300 mm ~~(22/40´)~~.

10. (Currently amended) The device according to claim 9 ~~c h a r a c t e r i s e d in that~~ wherein each nozzle is directed ~~in towards the centre of the stand pipe and obliquely downwards~~ at an angle relative to ~~the vertical and the~~ a direction of free fall of the fragmented pulp ~~granulate~~ of 45 ±15°.

11. (Currently amended) The device according to claim 10 ~~c~~ ~~h a r a c t e r i s e d i n that~~ wherein all nozzles are connected to a common distribution chamber ~~(60)~~ for dilution fluid, ~~which~~ the chamber is ~~pressurised~~ pressurized through a pressure-raising device ~~(61)~~.

12. (New) The device according to claim 7 wherein the nozzles are oriented obliquely downwardly.